Damage Mechanisms Affecting Fixed Equipment in the Refining Industry

API RECOMMENDED PRACTICE 571 SECOND EDITION, APRIL 2011



Damage Mechanisms Affecting Fixed Equipment in the Refining Industry

Downstream Segment

API RECOMMENDED PRACTICE 571 SECOND EDITION, APRIL 2011



Special Notes

API publications necessarily address problems of a general nature. With respect to particular circumstances, local, state, and federal laws and regulations should be reviewed.

Neither API nor any of API's employees, subcontractors, consultants, committees, or other assignees make any warranty or representation, either express or implied, with respect to the accuracy, completeness, or usefulness of the information contained herein, or assume any liability or responsibility for any use, or the results of such use, of any information or process disclosed in this publication. Neither API nor any of API's employees, subcontractors, consultants, or other assignees represent that use of this publication would not infringe upon privately owned rights.

API publications may be used by anyone desiring to do so. Every effort has been made by the Institute to assure the accuracy and reliability of the data contained in them; however, the Institute makes no representation, warranty, or guarantee in connection with this publication and hereby expressly disclaims any liability or responsibility for loss or damage resulting from its use or for the violation of any authorities having jurisdiction with which this publication may conflict.

API publications are published to facilitate the broad availability of proven, sound engineering and operating practices. These publications are not intended to obviate the need for applying sound engineering judgment regarding when and where these publications should be utilized. The formulation and publication of API publications is not intended in any way to inhibit anyone from using any other practices.

Any manufacturer marking equipment or materials in conformance with the marking requirements of an API standard is solely responsible for complying with all the applicable requirements of that standard. API does not represent, warrant, or guarantee that such products do in fact conform to the applicable API standard.

Users of this Recommended Practice should not rely exclusively on the information contained in this document. Sound business, scientific, engineering, and safety judgment should be used in employing the information contained herein.

API is not undertaking to meet the duties of employers, manufacturers, or suppliers to warn and properly train and equip their employees, and others exposed, concerning health and safety risks and precautions, nor undertaking their obligations to comply with authorities having jurisdiction.

Information concerning safety and health risks and proper precautions with respect to particular materials and conditions should be obtained from the employer, the manufacturer or supplier of that material, or the material safety data sheet.

All rights reserved. No part of this work may be reproduced, translated, stored in a retrieval system, or transmitted by any means, electronic, mechanical, photocopying, recording, or otherwise, without prior written permission from the publisher. Contact the Publisher, API Publishing Services, 1220 L Street, NW, Washington, DC 20005.

Foreword

Nothing contained in any API publication is to be construed as granting any right, by implication or otherwise, for the manufacture, sale, or use of any method, apparatus, or product covered by letters patent. Neither should anything contained in the publication be construed as insuring anyone against liability for infringement of letters patent.

Shall: As used in a standard, "shall" denotes a minimum requirement in order to conform to the specification.

Should: As used in a standard, "should" denotes a recommendation or that which is advised but not required in order to conform to the specification.

This document was produced under API standardization procedures that ensure appropriate notification and participation in the developmental process and is designated as an API standard. Questions concerning the interpretation of the content of this publication or comments and questions concerning the procedures under which this publication was developed should be directed in writing to the Director of Standards, American Petroleum Institute, 1220 L Street, NW, Washington, DC 20005. Requests for permission to reproduce or translate all or any part of the material published herein should also be addressed to the director.

Generally, API standards are reviewed and revised, reaffirmed, or withdrawn at least every five years. A one-time extension of up to two years may be added to this review cycle. Status of the publication can be ascertained from the API Standards Department, telephone (202) 682-8000. A catalog of API publications and materials is published annually by API, 1220 L Street, NW, Washington, DC 20005.

Suggested revisions are invited and should be submitted to the Standards Department, API, 1220 L Street, NW, Washington, DC 20005, standards@api.org.

TABLE OF CONTENTS

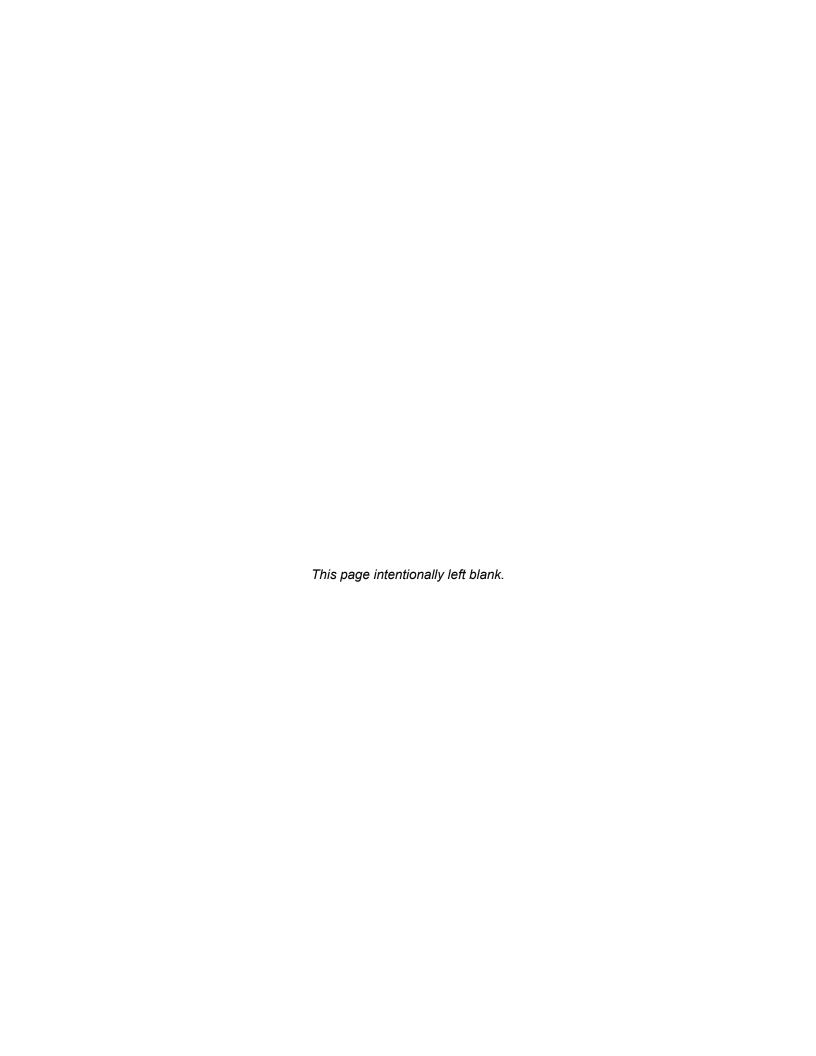
SECTION 1		1-1
	ntroduction	
	Scope	
1.3	Organization and Use	1-4
1.4 F	References	1-4
1.5 E	Definitions of Terms	1-4
	echnical Inquires	
SECTION 2		
-	Standards	
	Other References	
SECTION 3		
	Terms	
	Symbols and Abbreviations	
SECTION 4		
	Seneral	
	Mechanical and Metallurgical Failure Mechanisms	
4.2.1	Graphitization	
4.2.2	Softening (Spheroidization)	
4.2.3	Temper Embrittlement	
4.2.4	Strain Aging	
4.2.5	885°F (475°C) Embrittlement	
4.2.6	Sigma Phase Embrittlement	
4.2.7	Brittle Fracture	. 4-27
4.2.8	Creep and Stress Rupture	
4.2.9	Thermal Fatigue	
4.2.10	Short Term Overheating - Stress Rupture	.4-46
4.2.11	Steam Blanketing	.4-51
4.2.12	Dissimilar Metal Weld (DMW) Cracking	.4-54
4.2.13		
4.2.14		
4.2.15		
4.2.16		
4.2.17		
4.2.18	· · · · · · · · · · · · · · · · · · ·	
4.2.19		
	Gaseous Oxygen-Enhanced Ignition and Combustion	
	Jniform or Localized Loss of Thickness	
4.3.1	Galvanic Corrosion	
4.3.2	Atmospheric Corrosion	
4.3.2	Corrosion Under Insulation (CUI)	4-105 4 400
4.3.3 4.3.4	Cooling Water Corrosion	
_	Boiler Water Condensate Corrosion	
4.3.5		_
4.3.6	CO ₂ Corrosion	4-124
4.3.7	Flue-Gas Dew-Point Corrosion	4-128
4.3.8	Microbiologically Induced Corrosion (MIC)	
4.3.9	Soil Corrosion	
4.3.10	Caustic Corrosion	_
4.3.11	Dealloying	
	Graphitic Corrosion	
4.4 F	ligh Temperature Corrosion [>400°F (204°C)]	
4.4.1	Oxidation	4-153
4.4.2	Sulfidation	
4.4.3	Carburization	4-166

4.4.4 Decarburization	4-169
4.4.5 Metal Dusting	
4.4.6 Fuel Ash Corrosion	
4.4.7 Nitriding	
4.5 Environment – Assisted Cracking	
4.5.1 Chloride Stress Corrosion Cracking (CI'SCC)	4-184
4.5.2 Corrosion Fatigue	
4.5.3 Caustic Stress Corrosion Cracking (Caustic Embrittlement)	4-199
4.5.4 Ammonia Stress Corrosion Cracking	
4.5.5 Liquid Metal Embrittlement (LME)	4-210
4.5.6 Hydrogen Embrittlement (HE)	4-215
4.5.7 Ethanol Stress Corrosion Cracking (SCC)	4-220
4.5.8 Sulfate Stress Corrosion Cracking	
SECTION 5	
5.1 General	
5.1.1 Uniform or Localized Loss in Thickness Phenomena	
5.1.1.1 Amine Corrosion	
5.1.1.2 Ammonium Bisulfide Corrosion (Alkaline Sour Water)	
5.1.1.3 Ammonium Chloride Corrosion	
5.1.1.4 Hydrochloric Acid (HCI) Corrosion	5-16
5.1.1.5 High Temp H ₂ /H ₂ S Corrosion	
5.1.1.6 Hydrofluoric (HF) Acid Corrosion	
5.1.1.7 Naphthenic Acid Corrosion (NAC)	
5.1.1.8 Phenol (Carbolic Acid) Corrosion	
5.1.1.9 Phosphoric Acid Corrosion	
5.1.1.10 Sour Water Corrosion (Acidic)	
5.1.1.11 Sulfuric Acid Corrosion	5-41
5.1.1.12 Aqueous Organic Acid Corrosion	
5.1.2 Environment-Assisted Cracking	
5.1.2.1 Polythionic Acid Stress Corrosion Cracking (PASCC)	
5.1.2.2 Amine Stress Corrosion Cracking	5-55
5.1.2.3 Wet H ₂ S Damage (Blistering/HIC/SOHIC/SSC)	
5.1.2.4 Hydrogen Stress Cracking - HF	
5.1.2.5 Carbonate Stress Corrosion Cracking (ACSCC)	
5.1.3 Other Mechanisms	
5.1.3.1 High Temperature Hydrogen Attack (HTHA)	
5.1.3.2 Titanium Hydriding	
5.2 Process Unit PFD's	
ANNNEX A	
A.1 Introduction	_
A.2 Inquiry Format	A-3

SECTION 1

INTRODUCTION AND SCOPE

1.1	Introduction	1-3
	Scope	
1.3	Organization and Use	1-4
	References	
1.5	Definitions of Terms	1-4
	Technical Inquires	



1.1 Introduction

The ASME and API design codes and standards for pressurized equipment provide rules for the design, fabrication, inspection, and testing of new pressure vessels, piping systems, and storage tanks. These codes do not address equipment deterioration while in service and that deficiencies due to degradation or from original fabrication may be found during subsequent inspections. Fitness-For-Service (FFS) assessments are quantitative engineering evaluations that are performed to demonstrate the structural integrity of an in-service component containing a flaw or damage. The first step in a fitness-for-service assessment performed in accordance with API 579-1/ASME FFS-1 is to identify the flaw type and the cause of damage. Proper identification of damage mechanisms for components containing flaws or other forms of deterioration is also the first step in performing a Risk-Based Inspection (RBI) in accordance with API RP 580.

When conducting an FFS assessment or RBI study, it is important to determine the cause(s) of the damage or deterioration observed, or anticipated, and the likelihood and degree of further damage that might occur in the future. Flaws and damage that are discovered during an in-service inspection can be the result of a pre-existing condition before the component entered service and/or could be service-induced. The root causes of deterioration could be due to inadequate design considerations including materials selection and design details, or the interaction with aggressive environments/conditions that the equipment is subjected to during normal service or during transient periods.

One factor that complicates an FFS assessment or RBI study for refining and petrochemical equipment is that material/environmental condition interactions are extremely varied. Refineries and chemical plants contain many different processing units, each having its own combination of aggressive process streams and temperature/pressure conditions. In general, the following types of damage are encountered in petrochemical equipment:

- a) General and local metal loss due to corrosion and/or erosion
- b) Surface connected cracking
- c) Subsurface cracking
- d) Microfissuring/microvoid formation
- e) Metallurgical changes

Each of these general types of damage may be caused by a single or multiple damage mechanisms. In addition, each of the damage mechanisms occurs under very specific combinations of materials, process environments, and operating conditions.

1.2 Scope

This recommended practice provides general guidance as to the most likely damage mechanisms affecting common alloys used in the refining and petrochemical industry and is intended to introduce the concepts of service-induced deterioration and failure modes. These guidelines provide information that can be utilized by plant inspection personnel to assist in identifying likely causes of damage; to assist with the development of inspection strategies; to help identify monitoring programs to ensure equipment integrity.

The summary provided for each damage mechanism provides the fundamental information required for an FFS assessment performed in accordance with API 579-1/ASME FFS-1 or an RBI study performed in accordance with API RP 580.

The damage mechanisms in this recommended practice cover situations encountered in the refining and petrochemical industry in pressure vessels, piping, and tankage. The damage mechanism descriptions are not intended to provide a definitive guideline for every possible situation that may be encountered, and the reader may need to consult with an engineer familiar with applicable degradation modes and failure mechanisms, particularly those that apply in special cases.